EAST Search History

Ref #	Hits	Search Query	DBs	Default Operator	Plurals	Time Stamp
L1	12	US-5536699-\$.DID. OR US-5470542-\$. DID. OR US-5417939-\$.DID. OR US-5770770-\$.DID. OR US-5113015-\$. DID. OR US-4352940-\$.DID.	US-PGPUB; USPAT; EPO; JPO; DERWENT	OR	ON	2006/12/18 08:11
L2	31	"0127062"	US-PGPUB; USPAT; EPO; JPO; DERWENT	OR	ON	2006/12/18 08:45
L3	1247	reactive adj distillation	US-PGPUB; USPAT; EPO; JPO; DERWENT	OR	ON	2006/12/18 08:46
L4	204	prereactor	US-PGPUB; USPAT; EPO; JPO; DERWENT	OR	ON	2006/12/18 08:47
L5	9	l3 same l4	US-PGPUB; USPAT; EPO; JPO; DERWENT	OR	ON	2006/12/18 09:47
L7	681	562/606.ccls.	US-PGPUB; USPAT; EPO; JPO; DERWENT	OR ·	ON .	2006/12/18 09:47
L8	4	13 and 17	US-PGPUB; USPAT; EPO; JPO; DERWENT	OR	ON	2006/12/18 09:47

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                 CAS REGISTRY (SM) no longer includes Concord 3D coordinates
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         SEP 25
                 CAS REGISTRY (SM) updated with amino acid codes for pyrrolysine
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                 CEABA-VTB classification code fields reloaded with new
NEWS 11
                 classification scheme
NEWS 12
         OCT 19
                 LOGOFF HOLD duration extended to 120 minutes
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                 multiple databases
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                 The Derwent World Patents Index suite of databases on STN
                 has been enhanced and reloaded
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         NOV 10
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NEWS 19
        NOV 10
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                 8.01c now available
        NOV 13
                 CA/CAplus pre-1967 chemical substance index entries enhanced
NEWS 21
                 with preparation role
                 CAS Registry Number crossover limit increased to 300,000 in
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        NOV 20
                 additional databases
                 CA/CAplus to MARPAT accession number crossover limit increased
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                 to 50,000
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NEWS 25 DEC 11
                 CAS REGISTRY chemical nomenclature enhanced
        DEC 14
                 WPIDS/WPINDEX/WPIX manual codes updated
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NEWS 27
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=> reactive Distill?

300835 REACTIVE

151 REACTIVES

300940 REACTIVE

(REACTIVE OR REACTIVES)

119520 DISTILL?

164541 DISTD

1 DISTDS

164541 DISTD

(DISTD OR DISTDS)

25950 DISTG

176262 DISTN

1781 DISTNS

177001 DISTN

(DISTN OR DISTNS)

376913 DISTILL?

(DISTILL? OR DISTD OR DISTG OR DISTN)

L1 1117 REACTIVE DISTILL?

(REACTIVE (W) DISTILL?)

=> prereact?

L2 1428 PREREACT?

=> **11(1)12**

L3 4 L1 (L) L2

=> d 13 1-4 ti

- L3 ANSWER 1 OF 4 CAPLUS COPYRIGHT 2006 ACS on STN
- TI Method for producing dimethyl carbonate and ethylene glycol from ethylene carbonate and methanol continuously using pre-reactor
- L3 ANSWER 2 OF 4 CAPLUS COPYRIGHT 2006 ACS on STN
- TI Esterification of a Fatty Acid by Reactive Distillation
- L3 ANSWER 3 OF 4 CAPLUS COPYRIGHT 2006 ACS on STN
- TI Conceptual design aspects of reactive distillation processes for ideal binary mixtures
- L3 ANSWER 4 OF 4 CAPLUS COPYRIGHT 2006 ACS on STN
- TI Application of a fluidized reaction-distillation column for hydrolysis of methyl acetate

=> d 13 2-4 ti fbib abs

- L3 ANSWER 2 OF 4 CAPLUS COPYRIGHT 2006 ACS on STN
- TI Esterification of a Fatty Acid by Reactive Distillation
- AN 2003:469513 CAPLUS
- DN 139:181931
- TI Esterification of a Fatty Acid by Reactive Distillation
- AU Steinigeweg, Sven; Gmehling, Juergen
- CS Carl von Ossietzky University of Oldenburg, Industrial Chemistry, Oldenburg, D-26111, Germany
- SO Industrial & Engineering Chemistry Research (2003), 42(15), 3612-3619 CODEN: IECRED; ISSN: 0888-5885
- PB American Chemical Society
- DT Journal
- LA English
- OS CASREACT 139:181931
- A reactive distillation process for the production of decanoic AB acid Me esters by esterification of the fatty acid decanoic acid with methanol is presented. The reaction was catalyzed heterogeneously by a strong acidic ion-exchange resin (Amberlyst 15). A pragmatic kinetic model based on a Langmuir-Hinshelwood-Hougen-Watson approach was derived and the kinetic consts. of this and a pseudohomogeneous model were fitted. Two different catalytic packings, Katapak-S and Katapak-SP, were used for reactive distillation expts. The separation efficiency of Katapak-SP was determined exptl. and reactive distillation expts. in pilot-plant columns were performed. Operation conditions were varied (reflux ratio and reactant ratio) exptl. An equilibrium stage model is capable of describing the expts. quant. when the adsorption based a kinetic model is applied. Simulation was used subsequently to determine the influence of important operating and design factors (reactant ratio, reflux ratio, pressure, distillate-to-feed ratio, size of the reactive section, and role of a prereactor) and to compare the packings systematically. Finally, a process is proposed that is promising for scale-up and optimization with regard to economic issues.
- RE.CNT 17 THERE ARE 17 CITED REFERENCES AVAILABLE FOR THIS RECORD ALL CITATIONS AVAILABLE IN THE RE FORMAT
- L3 ANSWER 3 OF 4 CAPLUS COPYRIGHT 2006 ACS on STN
- TI Conceptual design aspects of reactive distillation processes for ideal binary mixtures
- AN 2002:874569 CAPLUS
- DN 138:58144
- TI Conceptual design aspects of reactive distillation processes for ideal binary mixtures
- AU Sundmacher, Kai; Qi, Zhiwen
- CS Max-Planck-Institut fuer Dynamik komplexer technischer Systeme, Magdeburg, D-39106, Germany

- SO Chemical Engineering and Processing (2003), 42(3), 191-200 CODEN: CENPEU; ISSN: 0255-2701
- PB Elsevier Science B.V.
- DT Journal
- LA English
- AB A comparative study on the conceptual design of reactive distillation process configurations is presented, considering the reversible reaction A1 + A2 in an ideal binary mixture as simple model system. The analyzed flow schemes are a reactor-distillation column sequence with an external recycle loop, the same recycle system with a prereactor, a nonreactive distillation column on top of a reactive reboiler, a fully reactive distillation column, and a hybrid distillation column combining a reactive and a nonreactive section. For these configurations, the design aspects are discussed in terms of the most important operating parameters, kinetic parameters and design parameters.
- RE.CNT 28 THERE ARE 28 CITED REFERENCES AVAILABLE FOR THIS RECORD ALL CITATIONS AVAILABLE IN THE RE FORMAT
- L3 ANSWER 4 OF 4 CAPLUS COPYRIGHT 2006 ACS on STN
- TI Application of a fluidized reaction-distillation column for hydrolysis of methyl acetate
- AN 1997:373867 CAPLUS
- DN 127:83057
- TI Application of a fluidized reaction-distillation column for hydrolysis of methyl acetate
- AU Han, S. J.; Jin, Y.; Yu, Z. Q.
- CS Department of Chemical Engineering, Tsinghua University, Beijing, 100084, Peop. Rep. China
- SO Chemical Engineering Journal (Lausanne) (1997), 66(3), 227-230 CODEN: CMEJAJ; ISSN: 1385-8947
- PB Elsevier
- DT Journal
- LA English
- A method for hydrolysis of MeOAc, a byproduct of poly(vinyl alc.) production, consists of a prereactor and a reactive distn
 . column. The operating variables, including the feed rate, feed ratio of water to MeOAc and reflux ratio, were investigated. The conversion of MeOAc increases with increasing reflux ratio, but decreases with increasing feed rate. The feed ratio of water to MeOAc has a considerable effect on the conversion of MeOAc, and an optimum feed ratio was determined

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